# Additives to Increase Fuel Heat Sink Capacity

### 41st AIAA/ASME/SAE/ASEE Joint Propulsion Conference

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July 11, 2005

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| maintaining the data needed, and c<br>including suggestions for reducing  | lection of information is estimated to<br>completing and reviewing the collect<br>this burden, to Washington Headqu<br>uld be aware that notwithstanding an<br>DMB control number. | ion of information. Send comments arters Services, Directorate for Information | regarding this burden estimate mation Operations and Reports | or any other aspect of the s, 1215 Jefferson Davis | nis collection of information,<br>Highway, Suite 1204, Arlington |
|---|--|--|--|--|--|
| 1. REPORT DATE  JUL 2005  |  | 2. REPORT TYPE   |  | 3. DATES COVERED <b>00-00-2005 to 00-00-2005</b>   |  |
| 4. TITLE AND SUBTITLE   |  | 5a. CONTRACT NUMBER  |  |  |  |
| Additives to Increase Fuel Heat Sink Capacity   |  |  |  | 5b. GRANT NUMBER                                   |  |
|   |  |  |  | 5c. PROGRAM ELEMENT NUMBER                         |  |
| 6. AUTHOR(S)  |  |  |  | 5d. PROJECT NUMBER                                 |  |
|   |  |  |  | 5e. TASK NUMBER                                    |  |
|   |  |  |  | 5f. WORK UNIT NUMBER                               |  |
| 7. PERFORMING ORGANIZATION NAME(S) AND ADDRESS(ES) <b>TDA Research Inc,12345 West 52nd Avenue,Wheat Ridge,CO,80033-1916</b> |  |  |  | 8. PERFORMING ORGANIZATION<br>REPORT NUMBER        |  |
| 9. SPONSORING/MONITORING AGENCY NAME(S) AND ADDRESS(ES)   |  |  |  | 10. SPONSOR/MONITOR'S ACRONYM(S)                   |  |
|   |  |  |  | 11. SPONSOR/MONITOR'S REPORT<br>NUMBER(S)          |  |
| 12. DISTRIBUTION/AVAIL Approved for publ  | LABILITY STATEMENT<br>ic release; distributi   | ion unlimited  |  |  |  |
| 13. SUPPLEMENTARY NO <b>The original docum</b>  | otes<br>nent contains color i  | images.  |  |  |  |
| 14. ABSTRACT  |  |  |  |  |  |
| 15. SUBJECT TERMS   |  |  |  |  |  |
| 16. SECURITY CLASSIFIC  | 17. LIMITATION OF<br>ABSTRACT  | 18. NUMBER<br>OF PAGES   | 19a. NAME OF   |  |  |
| a. REPORT<br>unclassified   | b. ABSTRACT <b>unclassified</b>  | c. THIS PAGE unclassified  | ADSTRACT   | 36   | RESPONSIBLE PERSON   |

**Report Documentation Page** 

Form Approved OMB No. 0704-0188

#### **Overview**

- Application of endothermic fuels.
- Initiated thermal cracking reactions.
- Results of laboratory experiments to measure initiated heat sink capacity.
- Results obtained with pilot scale fuel/air heat exchanger.

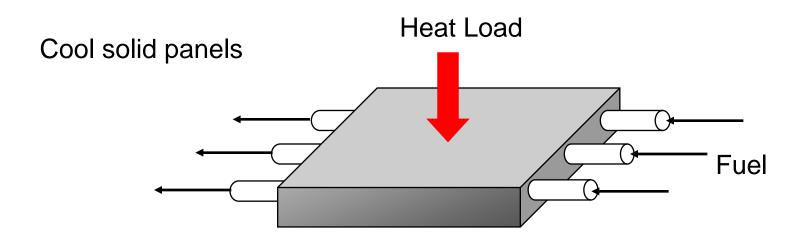


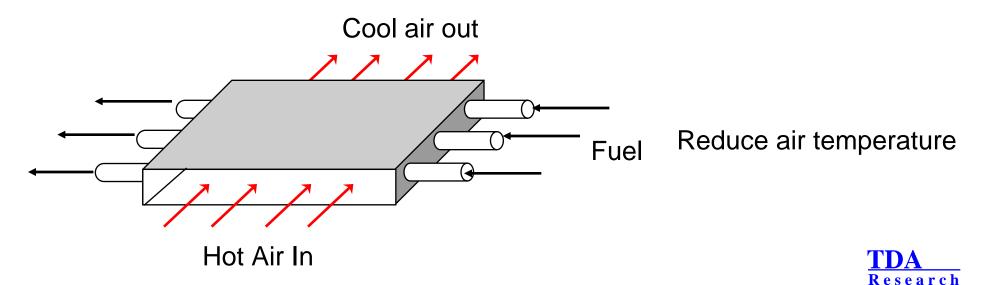
## NASA Application for Endothermic Fuels

- Improve commercial access to space.
  - Current cost is about \$10,000 per pound.
  - Goal is to reduce cost to \$100 per pound.
- Cost reductions will require:
  - Single stage to orbit (SSTO) vehicles.
  - Rocket-based combined cycle (RBCC) engines using hydrocarbon fuel.
- At speeds between Mach 5 and 10, heat loads exceed cooling available from sensible heating of the fuel.
- Thermal cracking reactions may provide the additional heat sink capacity.



## Applications of Endothermic Fuel Cooling





### **Thermal Cracking Reactions**

Heptane cracking.

$$C_7H_{16} \longrightarrow CH_4 + C_2H_4 + C_2H_6 + C_3H_6 + C_3H_8 + ...$$
  $\Delta H \approx +400 \text{ Btu/lb}$ 

Proceeds by a free radical mechanism.

Initiation - slow step

$$C_7H_{16} \rightarrow C_7H_{15} \cdot + H \cdot$$

Ethylene formation by  $\beta$  scission - fast

$$C_7H_{15} \bullet \to C_2H_4 + C_5H_{11} \bullet$$

Chain propagation - fast

$$C_7H_{16} + CH_3 \rightarrow C_7H_{15} + CH_4$$

 The overall rate is limited by the initiation step, which is slow at working temperatures.

#### **Addition of Chemical Initiator**

 Increases the rate of radical generation because the R-R bond is weaker than the C-H bond.

$$R-R_1 \rightarrow R \bullet + R_1 \bullet$$

R• and R₁• then react with the fuel.

$$R \bullet + C_7 H_{16} \rightarrow C_7 H_{15} \bullet + R-H$$

- The rest of the process is identical to the mechanism without the initiator.
  - The chemical initiator only starts the reaction it has no effect on reaction stoichiometry.
- Low concentrations required (less than 3 wt%).

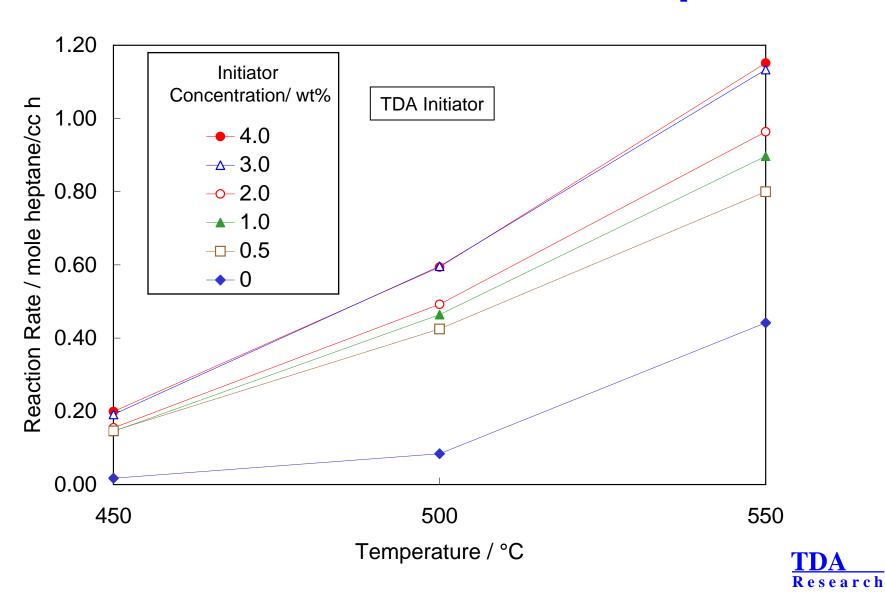


#### **Characteristics of the TDA Initiator**

- Consists of carbon, hydrogen, and oxygen.
- Is soluble in normal paraffin fuels.
- Is stable in its concentrated form at ambient temperatures.
- It is not a highly toxic chemical.



### **Previous Results with n-Heptane**

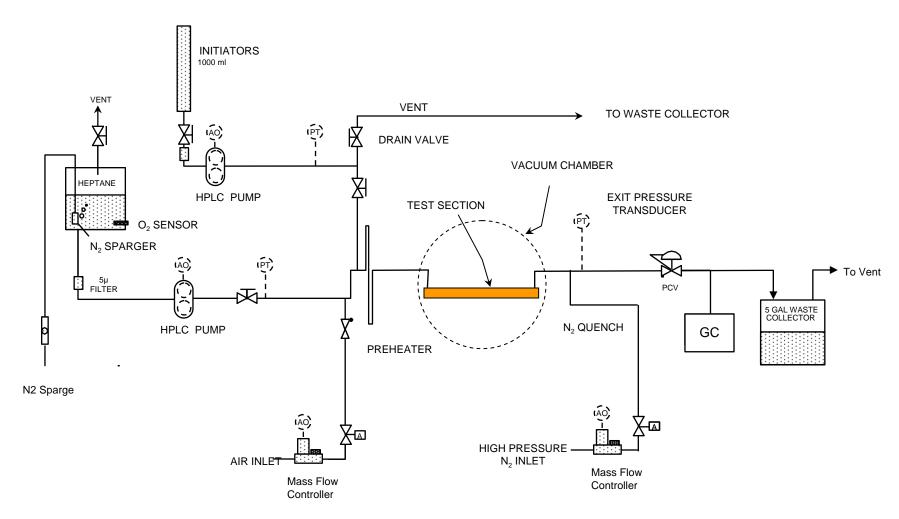


#### **Objective of Current Project**

- Measure heat sink capacity of real fuels such as JP-7 with and without initiator.
- Use kinetic data to design and construct a pilot scale heat exchanger and demonstrate initiator under realistic heat flux.

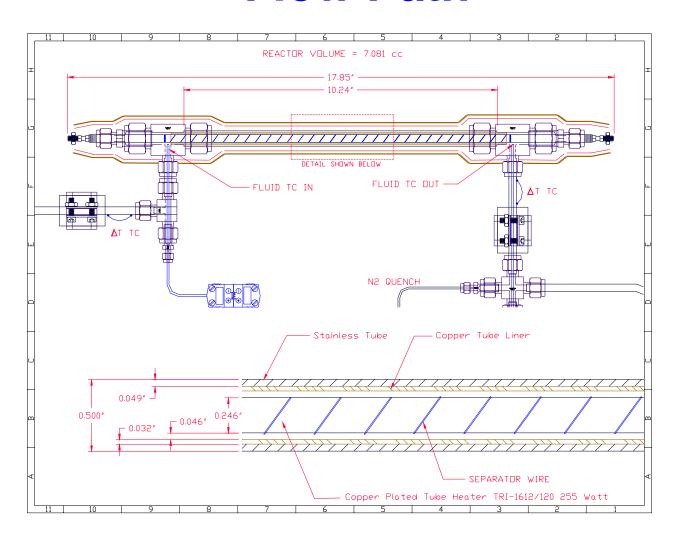


### **Laboratory Apparatus**



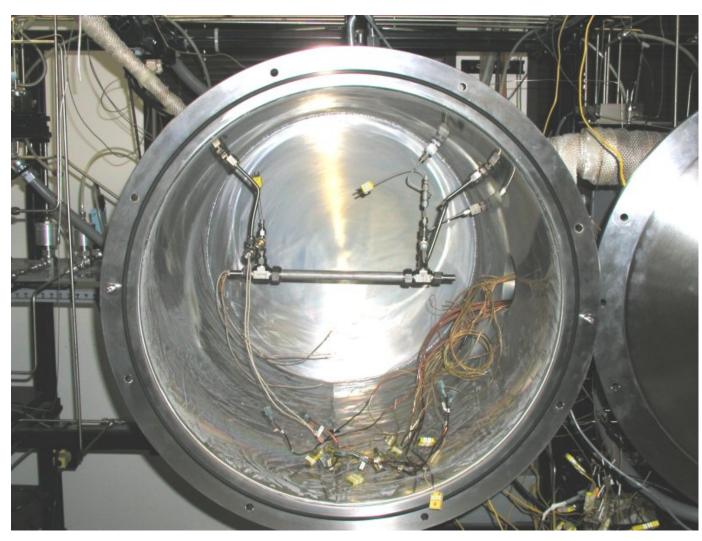


## Test Section Used Annular Fuel Flow Path



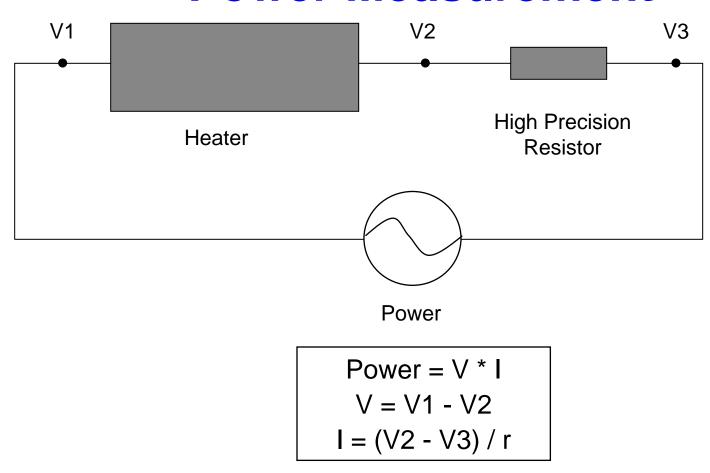


### **Test Section Installed in a Vacuum Chamber to Reduce Convective Losses**





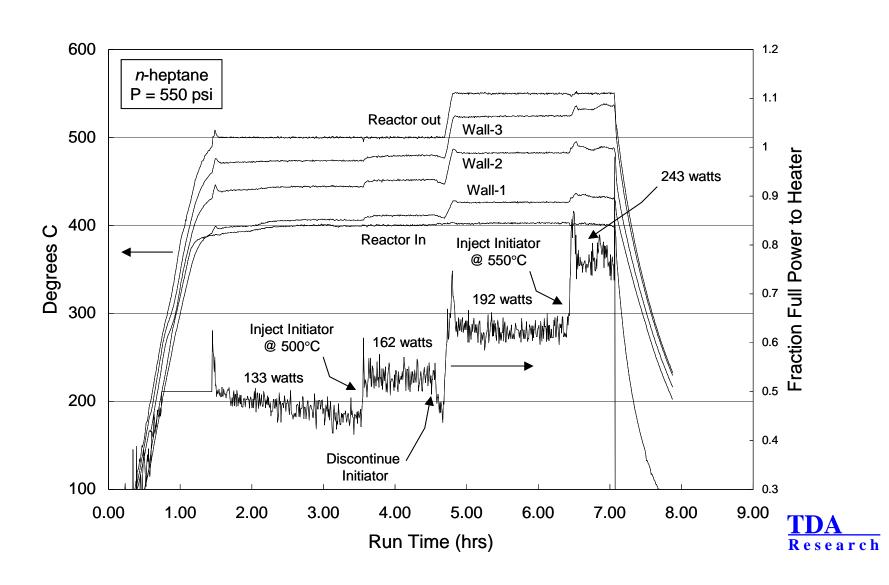
#### **Power Measurement**



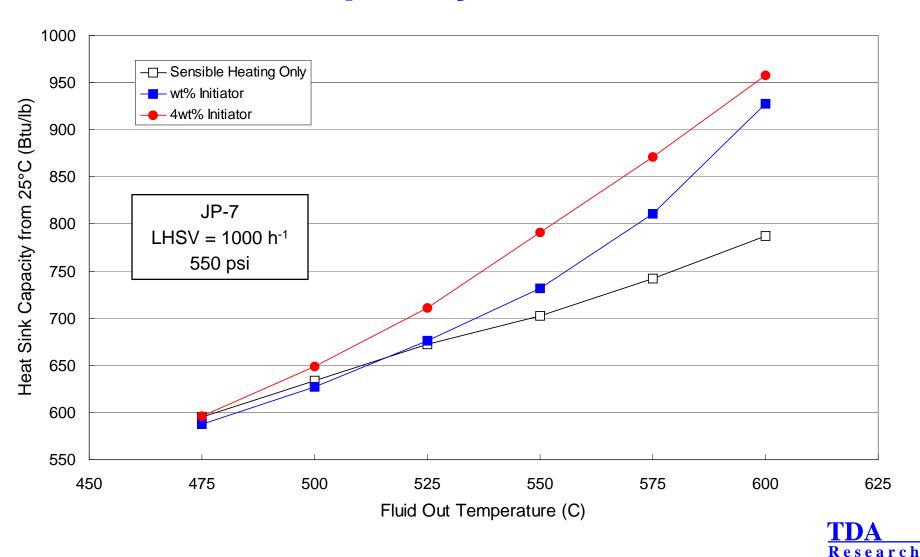
Measurements were made at 1000 Hz with a digital oscilloscope



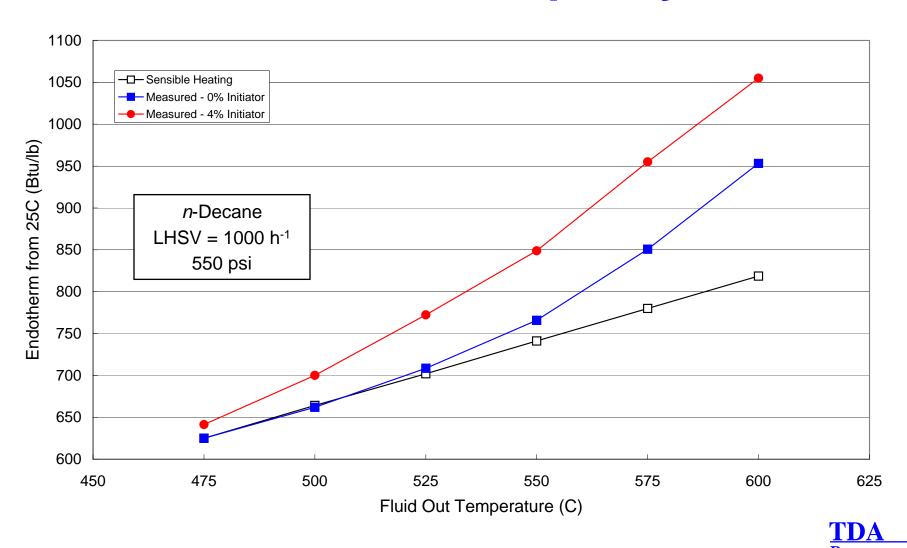
### Significant Power Increase with Initiator Addition



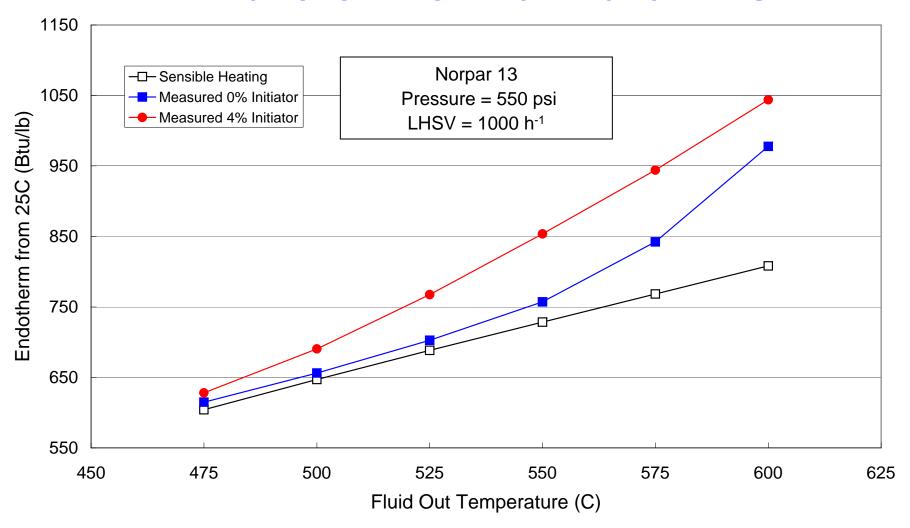
# The Initiator Improves the Heat Sink Capacity of JP-7



# Substantial Increases in *n*-Decane Heat Sink Capacity

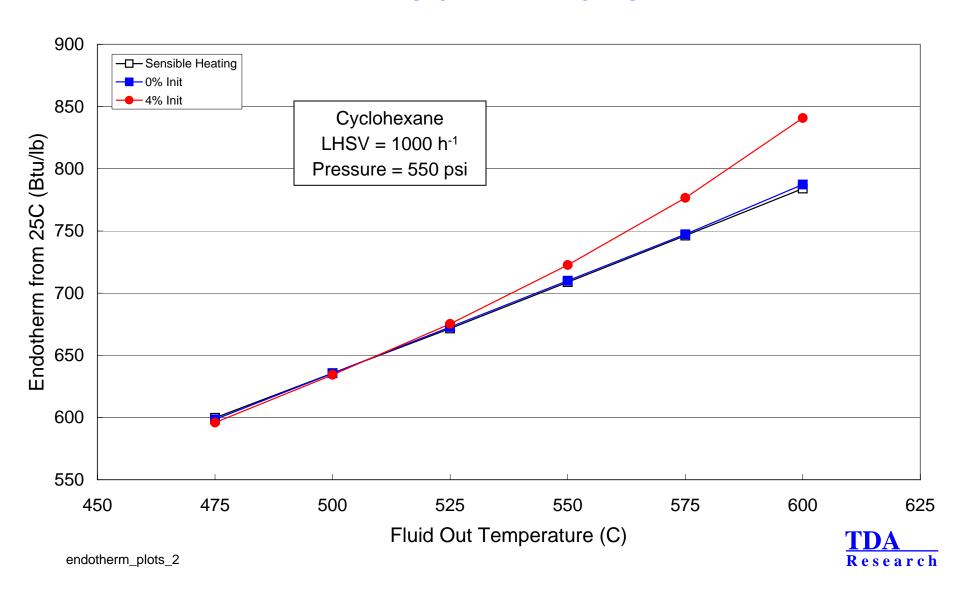


## The Initiator is Very Effective with a Mixture of Normal Paraffins

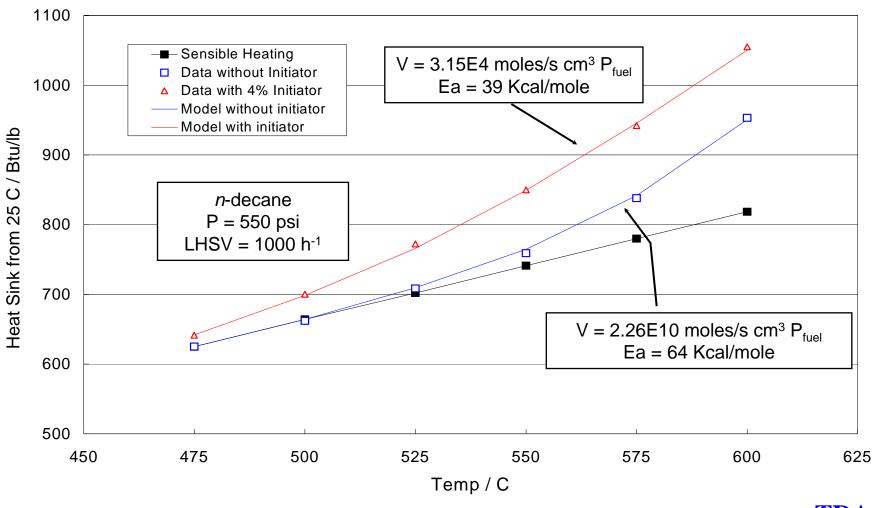




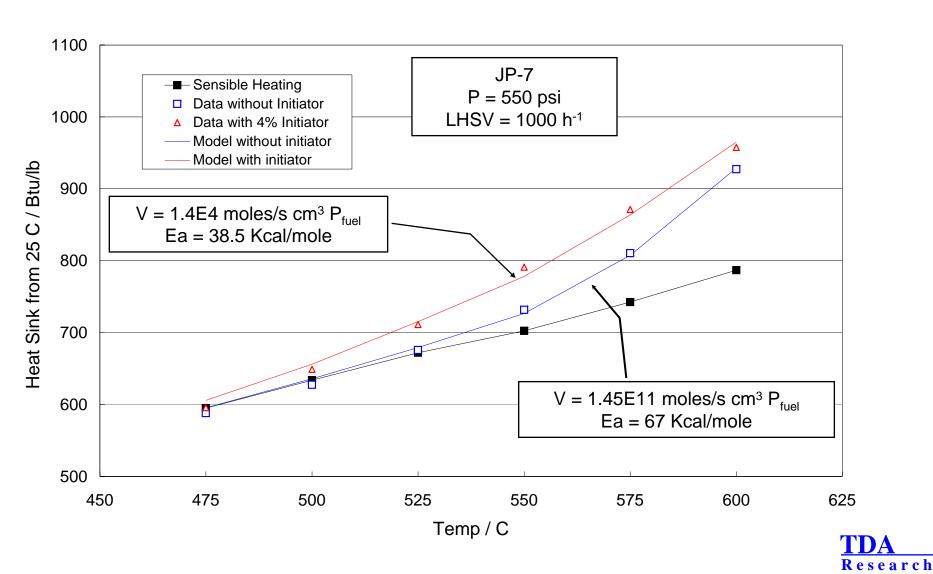
## Cyclohexane is Thermally Stable without Initiator



### The Initiator Reduces the Activation Energy of the Cracking Reaction



#### **Kinetic Data for JP-7**

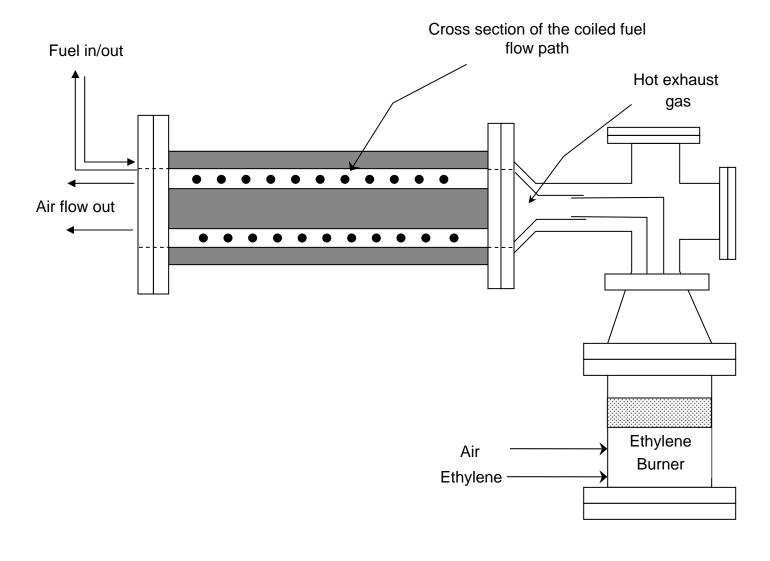


# Design and Construct Pilot Scale Air/Fuel Heat Exchanger

- Demonstrate heat sink capacity under realistic conditions.
- Heat flux of approximately 100,000 Btu/ft² h.
- $T_{air in} = 780$ °C,  $T_{air out} = 350$ °C
- $T_{\text{fuel in}} = 65^{\circ}\text{C}$ ,  $T_{\text{fuel out}} = 450^{\circ}\text{C}$



# Schematic of Ethylene Burner and the Heat Exchanger





### **Finned Inconel Tubing for Fuel**

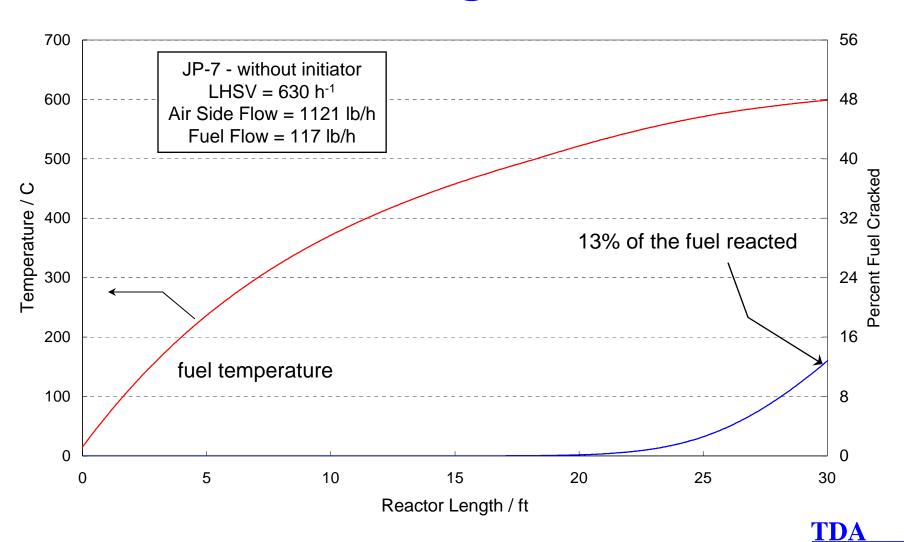




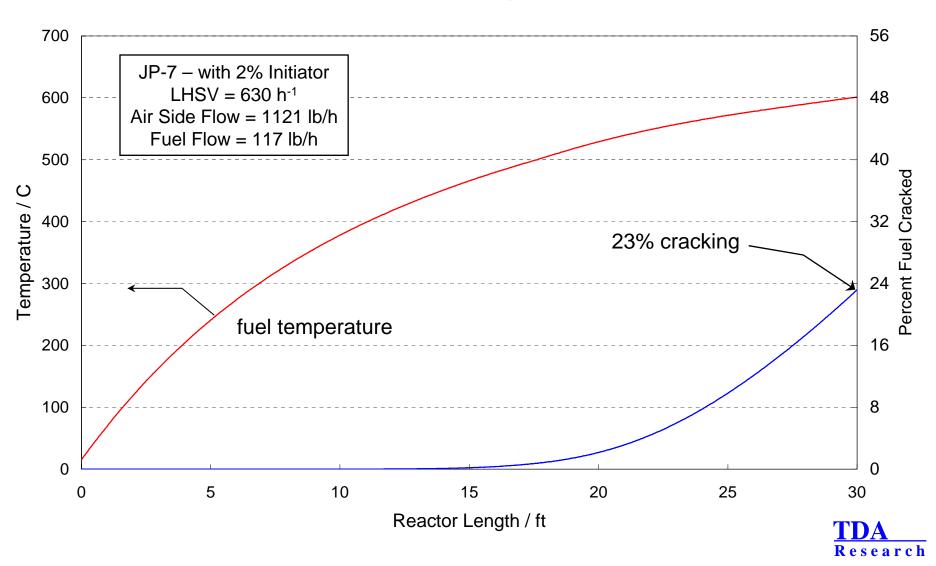
32 feet total finned tubing length
25.5 in overall unit length
3 in coil diameter
41 total wraps
~9.4 in length per wrap



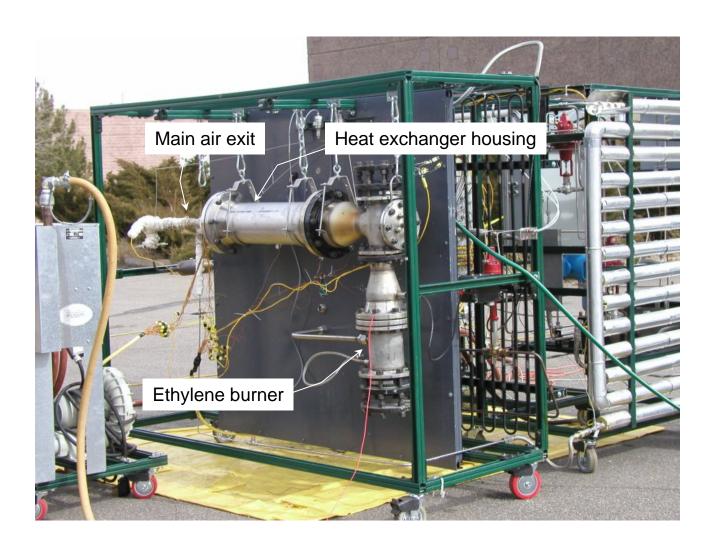
# Kinetic Model Used to Predict Cracking Level



# Addition of Initiator Increases the Fuel Cracking Reaction

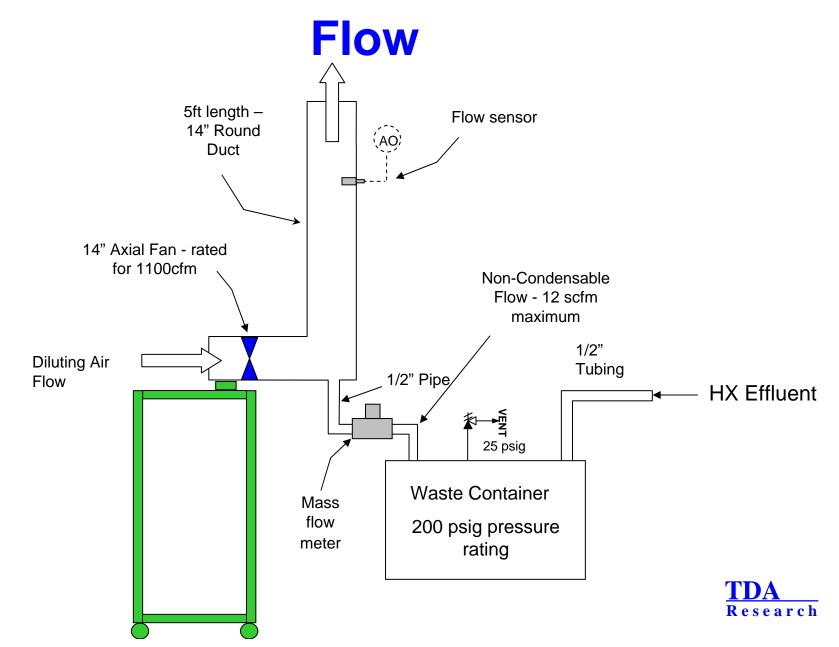


### **Installed in Test Rig**





#### We Measured Non Condensable

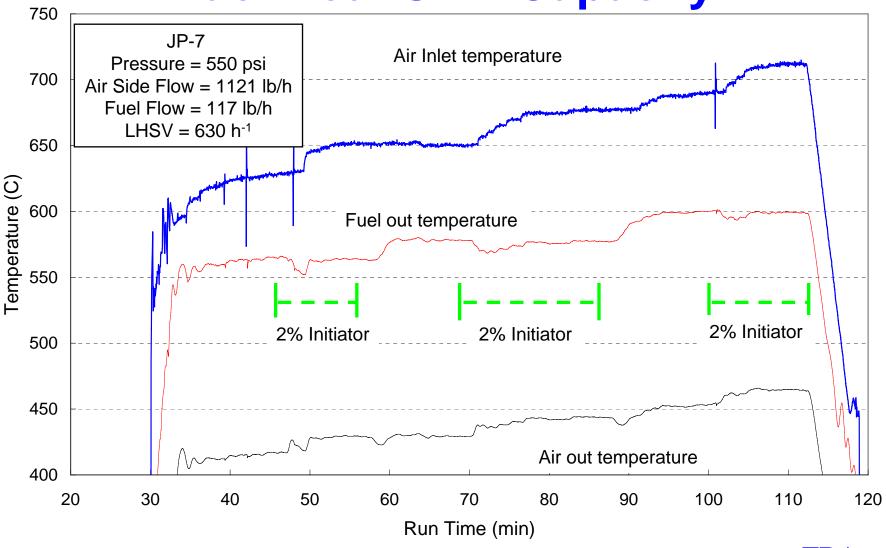


### **Pilot Scale Rig in Operation**

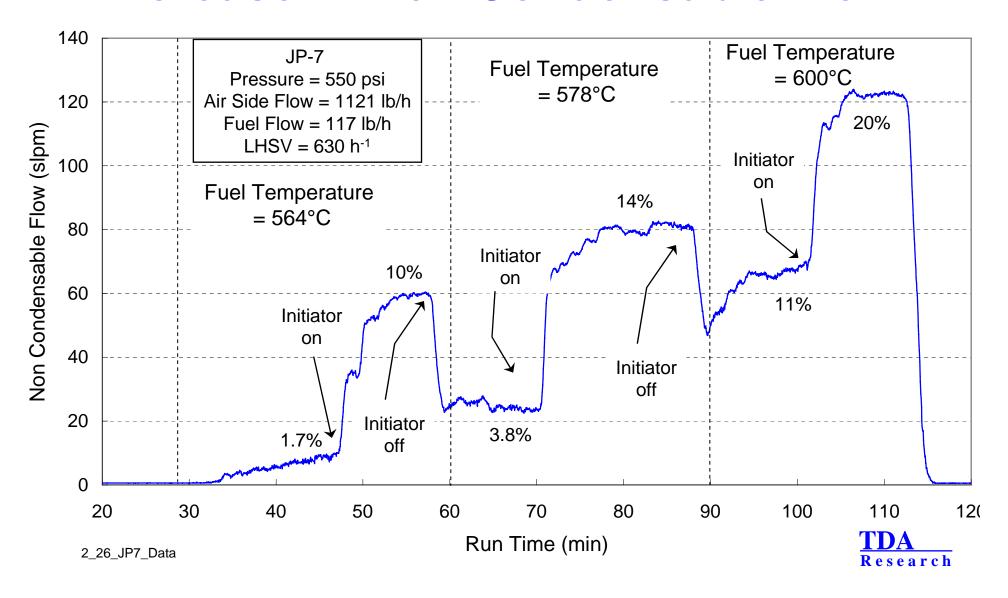




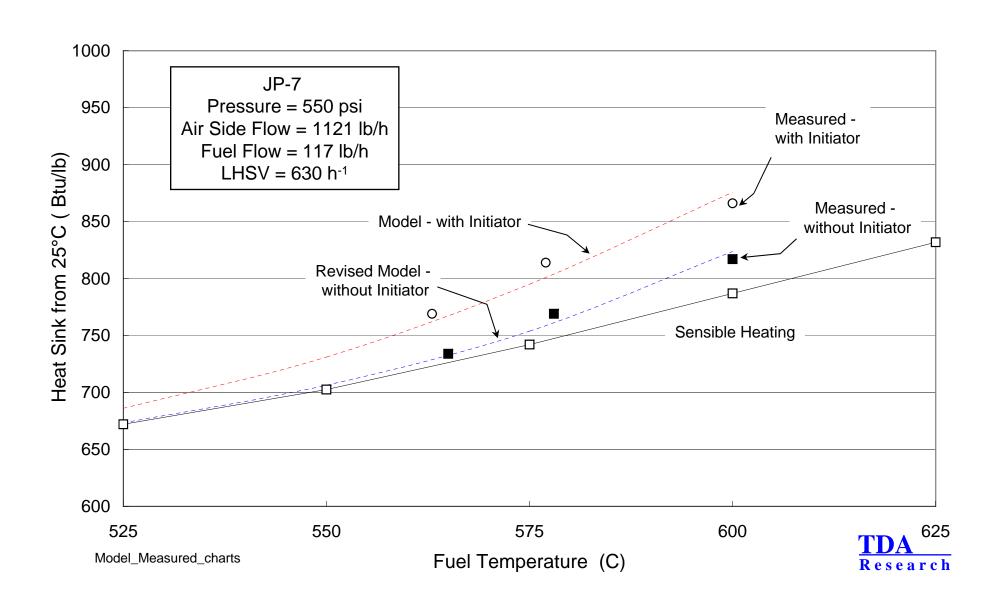
# Initiator Causes an Increase in the Fuel Heat Sink Capacity



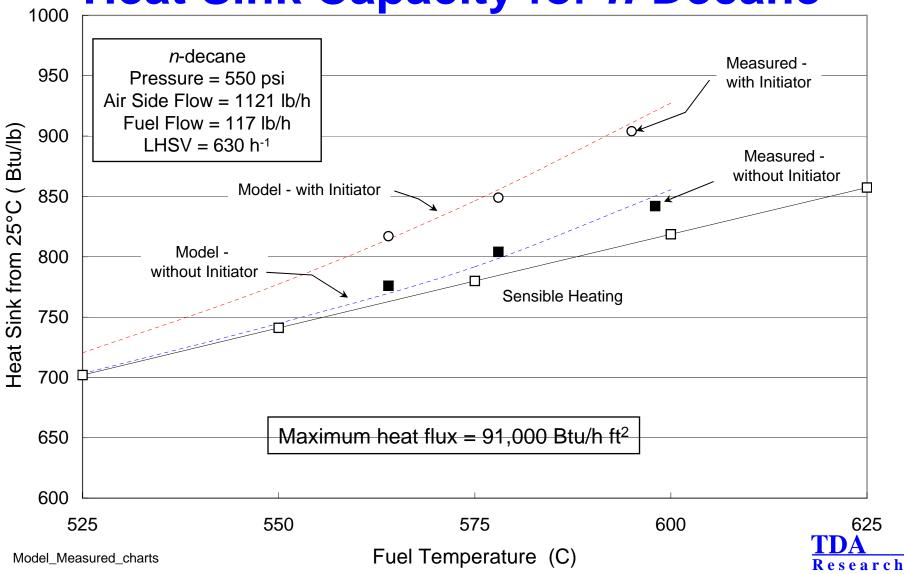
## Initiator Produces Significant Increase In Non Condensable Flow



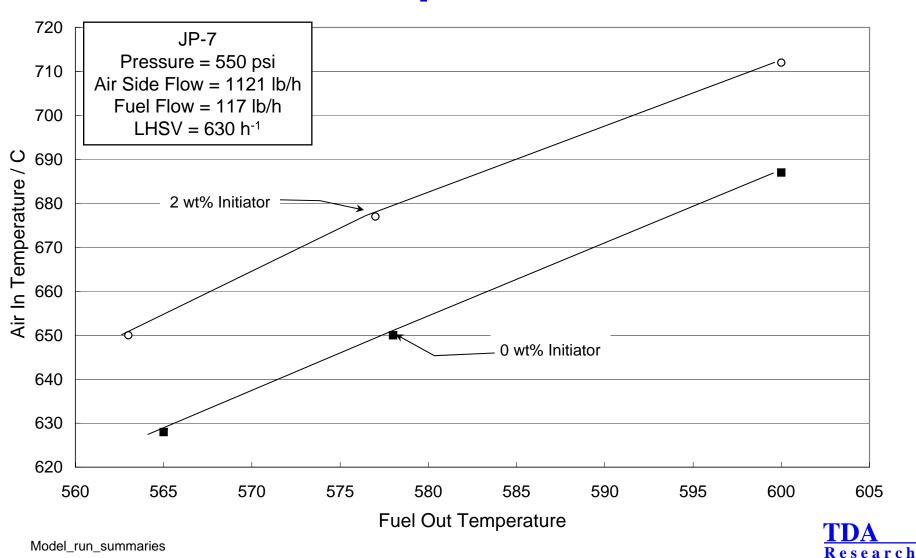
#### **Model for JP-7 Fits the Data Well**



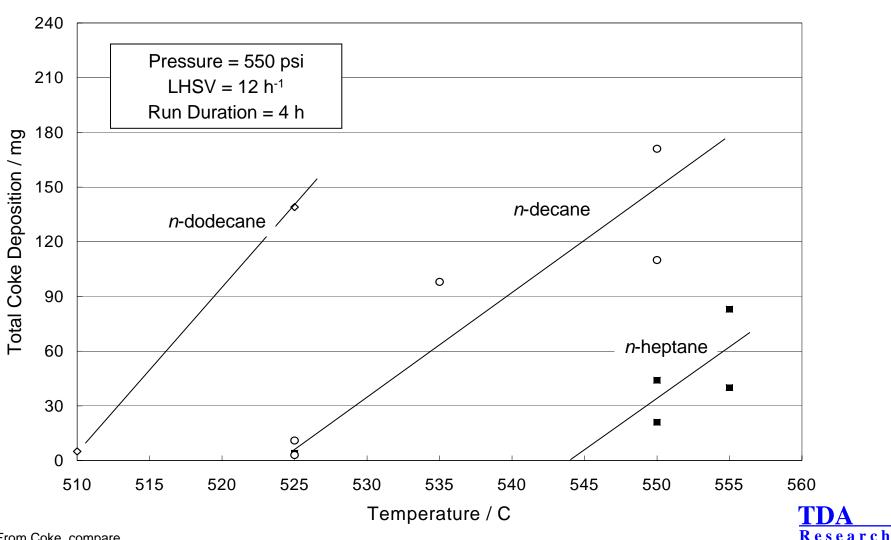
Initiated Cracking Adds Substantial Heat Sink Capacity for *n*-Decane



# The Initiator Can Reduce the HX Temperature



### **Coke Deposition Rates are a Strong Function of Temperature**



#### **Summary**

- The TDA initiator produces significant increases in the fuel heat sink capacities of JP-7 and model fuel compounds.
- The initiator reduces the activation energy for the thermal cracking reaction.
- We demonstrated the effectivness of the initiator in a fuel/air heat exchanger that operated at realistic heat flux.
- The initiator reduces the HX temperature, which could substantially reduce coke deposition.



#### **Acknowledgements**

- Funding provided by NASA SBIR Program, contract number NAS3-01039.
- Diane Linne, Contract Monitor.
- Air Force Research Laboratory for providing JP-7 fuel.

